

# Optimal digital control of an uncertain parameter 2nd order plant

Krzysztof Oprzędkiewicz<sup>a,\*</sup>

<sup>a</sup> Akademia Górniczo-Hutnicza, Al. A. Mickiewicza 30, 30-059 Kraków, Polska

## Article history:

Received 28 April 2018  
 Received in revised form  
 12 June 2018  
 Accepted 14 June 2018  
 Available online 27 June 2018

## Abstract

In the paper a construction of a control system for 2nd order, uncertain-parameter plant is discussed. The considered model of the plant is described by state space equation or by equivalent transfer function and it describes a huge class of real control plants, for example – electric drives or oriented PV systems. As a controller the digital proportional (P) controller was employed. The control system is going to be implemented at the microcontroller platform. Results are by the example depicted.

**Key words:** Digital control, optimal control, uncertain parameter systems

## Introduction

The minimum energy digital control has been one of main problems in control theory since many years. This problem has been presented for example in classic book Athans Falb (1966). Fundamentals of digital control are given by Isermann in 1989 and 1992, the modeling and control of uncertain parameter systems with two-dimensional uncertain parameter space have been analysed by Oprzędkiewicz and they are summarized in monograph from 2009, the control of this class of plants has been analysed for example by Mitkowski and Oprzędkiewicz in 2011 and 2012.

This paper is devoted to present the synthesis of digital control system for a class of uncertain parameter systems described by state equation or equivalent transfer function. The uncertain parameters of the plant are described by interval numbers. The control system is expected to assure the realization of servo control with minimal energy consumption. Results can be employed to control of the oriented PV system or another similar plant.

The paper is organized as follows: at the beginning the considered class of control plants is given. Next the discrete control system and its optimization are discussed. Finally the numerical example and final conclusions are presented.

## Materials and Methods

### The plant under consideration

The most general model of the plant under consideration is an uncertain-parameter, linear state space equation:

$$\begin{aligned} \dot{x}(t) &= A(q)x(t) + Bu(t) \\ y(t) &= Cx(t) \end{aligned} \quad (1)$$

In equation (1)  $x(t) \in R^2$ ,  $u(t) \in R$ ,  $y(t) \in R$ . A state matrix of the system is a Frobenius matrix, parameter  $q$  describes the uncertainty of the model and it is described by the positive interval number.

$$A(q) = \begin{bmatrix} 0 & 1 \\ 0 & -q \end{bmatrix} \quad (2)$$

where:

$$q = [\underline{q}, \bar{q}], \quad \underline{q} > 0 \quad (3)$$

Control and output matrices are well known and they are equal:

$$B = \begin{bmatrix} 0 \\ 1 \end{bmatrix} \quad C = [1 \quad 0] \quad (4)$$

A transfer function  $G(s, q) = C(sI - A(q))^{-1}B$  can be assigned with the use of (1) – (4) and it is a function of the uncertain parameter  $q$ :

$$G(s, q) = \frac{1}{s^2 + qs} \quad (5)$$

The plant described by (1)-(5) will be controlled with the use of discrete controller. This implies, that A/D and D/A converters working synchronically should be applied. The both elements build so called process interface. The scheme of the plant with both elements is shown in the figure 1.

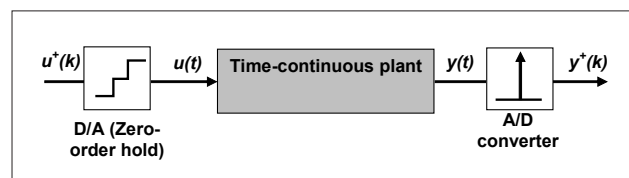


Figure 1. Continuous control plant with D/A and A/D converters

\*Corresponding author: kop@agh.edu.pl

To describe the discrete plant shown in figure 1 the continuous-time state space equation (1) – (4) should be transformed to the discrete form with the use of following relations:

$$A^+(q) = e^{T_s A(q)}, \quad B^+(q) = \int_0^{T_s} e^{A(q)t} B dt, \quad C^+ = C \quad (6)$$

A discrete transfer function of the plant shown in the Figure 1 is described as follows:

$$G^+(z) = C^+ (zI - A^+)^{-1} B^+ + D^+ \quad (7)$$

If the plant is described by the continuous transfer function (5), then the discrete transfer function (7) can be expressed as follows:

$$G^+(z) = (1 - z^{-1}) Z \left( \frac{G(s)}{s} \right) \quad (8)$$

The discrete transfer function (8) is a function of uncertain parameter  $q$  and the sample time  $T_s$  and it can be written in the form analogical to (5):

$$G^+(z, q, T_s) = \frac{v_1(q, T_s)z + v_0(q, T_s)}{z^2 + w_1(q, T_s)z + w_0(q, T_s)} \quad (9)$$

In (9)  $v$  and  $w$  denote coefficients of numerator and denominator of (9) respectively. They are equal:

$$\begin{aligned} w_1(q, T_s) &= -(1 + e^{-qT_s}) \\ w_0(q, T_s) &= e^{-qT_s} \\ v_1(q, T_s) &= \frac{1}{q} + \frac{1}{q^2} (1 + e^{-qT_s}) - \frac{2}{q^2} \\ v_0(q, T_s) &= \frac{1}{q^2} + \left( \frac{1}{q^2} - \frac{1}{q} \right) e^{-qT_s} \end{aligned} \quad (10)$$

During construction of a discrete system shown in Figure 1 and described by (9) – (10) a crucial problem is the proper selection of the sample time  $T_s$ . The properly set sample time should assure the proper work of the control system for each value of uncertain parameter of the plant, described by the parameter  $q$ .

The value of sample time  $T_s$  is determined both by the plant properties and the applied control algorithm. The sample time assign problem is one of fundamental in Control Theory and it was presented by many Authors, for example by Isermann (1989, 1992). Additionally, in the considered case the uncertainty of the discrete system should not be greater, than the uncertainty of the continuous system (see Oprzędkiewicz 2009).

**A closed-loop, discrete P control system**

The uncertain-parameter plant described above can be controlled with the use of digital controller. The general scheme of a discrete, closed – loop control system for plant under consideration is shown in the Figure 2.

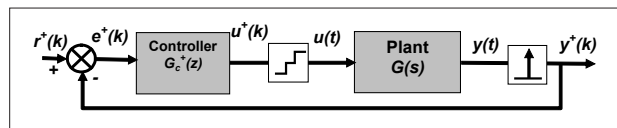


Figure 2. The closed-loop digital control system for the considered plant

In figure 2  $r^+(k)$  denotes a seat point,  $e^+(k)$  denotes discrete error,  $u^+(k)$  denotes discrete control signal,  $u(t)$  denotes continuous control signal,  $y(t)$  denotes a continuous process value and  $y^+(k)$  denotes the discrete process value.

For the control system shown in figure 2 an analytical relationship between „z” transform of the control system  $U^+(z)$ , “z” transform of seat point  $R^+(z)$  and transfer functions  $G_c^+(z)$  and  $G^+(z)$  can be given. It has the following form:

$$U^+(z) = \frac{G_c^+(z)}{1 + G^+(z)G_c^+(z)} \cdot R^+(z) \quad (11)$$

Assume, that to the control of the plant an ideal proportional (P) controller, described by the transfer function (12) should be applied:

$$G_c^+(z) = k_r \quad (12)$$

The proportional gain of the controller (12) should be assigned with respect to the following factors:

The closed-loop control system must be stable for each value of uncertain parameter of the system, described by the interval number  $q$ .

The cost function (described in the next section) for the control system should be minimal.

With respect to (11) and (12) the discrete control signal can be expressed as follows:

$$U^+(z) = \frac{k_r z^2 + k_r w_1(q, T_s)z + k_r w_0(q, T_s)}{z^2 + (w_1(q, T_s) + k_r v_1(q, T_s))z + (k_r v_0(q, T_s) + w_0(q, T_s))} \cdot R^+(z) \quad (13)$$

In (13)  $v$  and  $w$  denote coefficients of numerator and denominator. They are expressed by (10).

Furthermore, the discrete transfer function  $G_z^+(z) = Y^+(z)/R^+(z)$  of the discrete control system shown in Figure 2 is a function of uncertain parameter  $q$ , sample time  $T_s$  and gain  $k_r$ :

$$G_z^+(z, q, T_s, k_r) = \frac{Y^+(z)}{R^+(z)} = \frac{k_r v_1(q, T_s)z + k_r v_0(q, T_s)}{z^2 + (w_1(q, T_s) + k_r v_1(q, T_s))z + (k_r v_0(q, T_s) + w_0(q, T_s))} \quad (14)$$

The characteristic polynomial of the closed-loop system  $W(z)$  is also a function of uncertain parameter  $q$ , sample time  $T_s$  and gain  $k_r$ . It is equal:

$$W(z, q, T_s, k_r) = z^2 + (w_1(q, T_s) + k_r v_1(q, T_s))z + (k_r v_0(q, T_s) + w_0(q, T_s)) \quad (15)$$

Roots of polynomial (15) build a spectrum of closed-loop system  $\Lambda z^+$ , which can be defined as follows:

$$\Lambda_i^+(q, T_s, k_r) = \{ \lambda_i^+(q, T_s, k_r) : W(\lambda_i^+, q, T_s, k_r) = 0 \} \quad i = 1, 2 \quad (16)$$

The considered closed-loop control system is required to be practically implemented on the microcontroller platform. This implies, that the parameters of the discrete controller: sample time  $T_s$  and proportional gain  $k_r$  must be possible to physical realization onto particular hardware platform. The most simple notation of these boundaries is to write they as intervals (17):

$$\begin{aligned} \underline{k_r} \leq k_r \leq \overline{k_r}, \underline{k_r} > 0 \\ \underline{T_s} \leq T_s \leq \overline{T_s}, \underline{T_s} > 0 \end{aligned} \quad (17)$$

The both controller parameters build the vector  $p$  defined by (18):

$$p = [k_r \quad T_s]^T \quad (18)$$

where  $k_r$  and  $T_s$  are parameters possible to technical realization in particular platform. All vectors  $p$  build the space of controller parameters  $P$ , which is a subspace of  $R^3$ :

$$P = \{ p = [k_r, T_s]^T : \underline{k_r} < k_r \leq \overline{k_r}, \underline{T_s} \leq T_s \leq \overline{T_s} \} \subset R^3 \quad (19)$$

Set  $P$  defined by (19) can be interpreted as cube in space  $R^3$ .

The spectrum (16) with the respect to (18), (19) can be written as follows:

$$\Lambda_i^+(p, q) = \{ \lambda_i^+(p, q) : W(\lambda_i^+(p, q)) = 0, p \in P \} \quad i = 1, 2 \quad (20)$$

## Results and Discussion

### The stability discussion

The discrete transfer function (14) of the closed-loop control system is a function of parameters collected in the set  $P$  and uncertain parameter  $q$ . These parameters determine elementary possibilities of the considered control system. It is obvious, that the fundamental property of each control system is their stability.

In the considered case the sufficient and necessary condition of stability is, the whole spectrum of the system must be localized inside the unit circle. The meeting of this condition is determined by values of parameter  $q$  and controller parameters  $p \in P$  and it can be expected, that for certain values of  $p$  and  $q$  the control system will be stable and for other it will not be stable.

Vectors  $p$  assuring the stability of the system will be denoted by  $p_s$ , and set of all vectors  $p_s$  will be denoted by  $P_s$ . It can be expressed as follows:

$$P_s = \{ p \in P : |\lambda_i^+(q, p)| < 1 \} \quad i = 1, 2 \quad (21)$$

It is obvious, that  $P_s \subseteq P$ . The set  $P_s$  can be assigned analytically or numerically and it can be interpreted as three dimensional in  $R^3$ .

### The cost function

For the considered control system the classic servo control problem can be formulated: the process value  $y(t)$  should trace the set point  $r(t)$  with minimal possible energy consumption. A function describing the energy consumption in the discrete control system can be most simply expressed as follows:

$$J_1^+(p_s) = \sum_{k=0}^{\infty} (u^+(k))^2 \quad (22)$$

At this moment remember, that the control system is going to be implemented onto microcontroller platform. This assumption can be additionally applied to estimation the energy consumption in the system, because the energy consumption in microcontroller system increases with the speed of work. Furthermore, the unique measure of this speed is the sample time  $T_s$ : the smaller sample time denotes the bigger speed of the system.

In conclusion, the cost function for the considered control problem can be proposed as follows:

$$J_2^+(p_s, q) = h_1 \sum_{k=0}^{\infty} (u^+(k))^2 + h_2 \frac{1}{T_s} \quad (23)$$

where:

$u^+(k)$  – the discrete control signal in  $k$  – th step,

$T_s$  – the sample time,

$h_1, h_2$  – weight coefficients.

The cost function (27) is a function of plant parameter  $q$  and controller parameters:  $T_s$  and  $k_r$ .

Weight coefficients in the function (23) are assigned to describe detailed real situation – for example, if the more important is the speed of work the control system, the coefficient  $h_2$  is smaller, than the  $h_1$ .

### Geometric interpretation of the cost function

The cost function (23) is a function of uncertain plant parameter, described by the interval number  $q$  and controller parameters, expressed by vector  $p_s \in P_s$ . This implies, that the geometric interpretation of this function in the “visible” space  $R^3$  can be not simple. To make the geometric interpretation of function (23) possible to propose we can notice, that:

For the constant, selected value of the uncertain plant parameter  $q$  the cost function as a function of set  $P_s$  can be interpreted as a surface in the  $R^3$ .

Consequently, for all values of uncertain parameter  $q$ , described by an interval number  $[q, \overline{q}]$  the cost function can be interpreted as a body in  $R^3$  space, limited by border values of  $q$ .

The both above notes allow us to present the geometric interpretation of cost function (23). It is shown (for exemplary values of all parameters) in the figure 3.

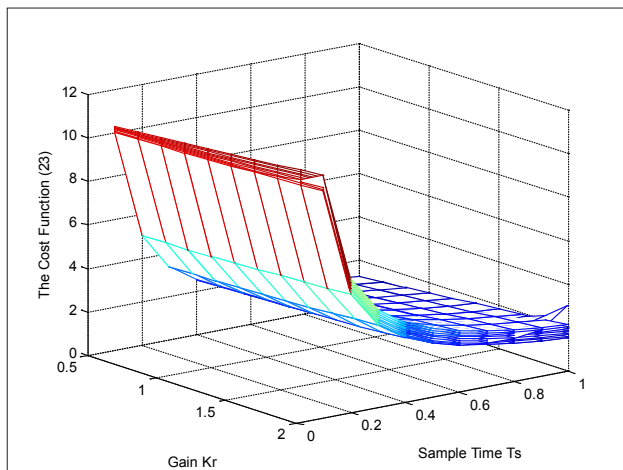


Figure 3. The geometric interpretation of the cost function (23)

**Remarks about the synthesis of an optimal controller**

After the whole above considerations the discrete control system synthesis problem can be formulated as follows:

Inside the set of controller parameters  $P_s$  should be found such values of sample time  $T_{s0}$  and gain  $k_{r0}$  for which the cost function (23) is minimal for each value of uncertain parameter  $q$ :

$$J_B^+(p_{s0}, q) \leq J_2^+(p_s, q), q \in Q \tag{24}$$

Notice, that for the fixed value of uncertain parameter  $q$  the cost function (23) is determined by controller parameters only.

The analytical formula of cost function (23) is possible to formulate, but it is extremely complicated and use it to minimum search is rather impossible. This implies, that the minimization of cost function (23) can be run with the use of numerical methods with support of geometric interpretation of cost function and additionally remark presented underneath.

**Remark 1**

Assumptions:

Consider the interval dynamic system described by (1) – (5),

The system is controlled with the use of discrete proportional controller with gain  $k_r$  and sample time  $T_s$ .

The ranges of controller parameters are also described by interval numbers and they generate the set of controller parameters  $P_s$  described by (21),

The uncertain parameter of the plant is described by interval number  $q$ .

Thesis:

For constant values of sample time  $T_s$  and uncertain parameter  $q$  the cost function (23) is an increasing function of controller gain  $k_r$

The proof of the above remark is presented underneath.

At the beginning notice, that the cost function (23) can be expressed in the following form:

$$J_2^+(p_s, q) = h_1 f_1(p_s, q) + h_2 f_2(p_s) \tag{25}$$

where:

$$f_1(p_s, q) = \sum_{k=0}^{\infty} (u^+(k))^2 \tag{26}$$

$$f_2(p_s) = \frac{1}{T_s} \tag{27}$$

The function  $f_1(p_s, q)$  described by (26) is a function both uncertain parameter  $q$  and controller vector  $p_s$ , the function  $f_2(p_s)$  is a function of sample time  $T_s$  only. This implies, that the function of proportional gain  $k_c$  is the function (26) only.

Next, in the case of continuous time the function (26) describing the energy consumption is expressed as the following integral:

$$I(q, k_c) = \int_0^{\infty} u^2(t) dt \tag{28}$$

The value of continuous integral (28) can be simply calculated analytically. It is equal:

$$I(q, k_c) = \frac{k_c(k_c + q)}{2q} \tag{29}$$

The function (29) does not have a minimum for positive  $q$  and positive  $k_c$  and it increases for increasing value of parameter  $k_c$  and it decreases for increasing value of the uncertain parameter  $q$ .

Furthermore, the continuous function (28) can be interpreted as a boundary case of discrete function (26). It can be expressed as follows:

$$I(q, k_r) = \lim_{T_s \rightarrow 0} I^+(q, k_r, T_s) \tag{30}$$

Finally, if the continuous function (28) is increasing for positive, increasing  $k_c$  and the equation (30) is kept, we can expect, that the discrete function (26) will behave analogically. This conclusion ends the proof.

**Example**

As an example consider the plant described by transfer function (5) with uncertain parameter described by interval number  $q = [1.0; 2.0]$ . For this plant we construct the discrete control system shown in figure 2. The set  $P_s$  of controller parameters assuring the stability of the closed-loop control system is described as underneath:

$$\begin{aligned} 0.1 \leq T_s \leq 1.0 \\ 0.5 \leq k_r \leq 2.0 \end{aligned} \tag{31}$$

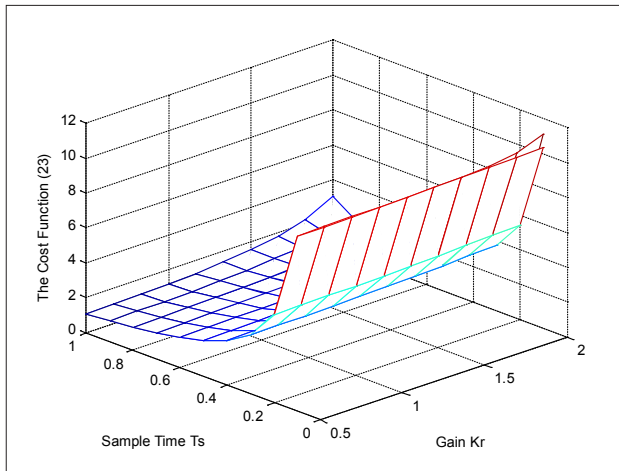
At the beginning a distribution of cost function (23) for ranges of controller parameters described by (31) was assigned. The cost function was calculated with the use of (23), both weight coefficients  $h_1$  and  $h_2$  were equal 1.0. The control function was

calculated with the use of equation (13), the step amplitude was equal 1.0. The distribution of cost function along the set  $P_s$  described by (31) is shown in Figure 3. The vertex values of cost function (23) are written in Table 1.

**Table 1.** The vertex values of cost function (23) in Example

	$T_s$	0.1	<b>1.0</b>	1.0	0.1
$q$	$k_r$	0.5	<b>0.5</b>	2.0	2.0
	1.0	10.0355	<b>1.0490</b>	3.0280	11.1175
	2.0	10.0602	<b>1.0639</b>	1.5317	10.4036

For both values of uncertain parameter  $q$  the minimum of the cost function (23) for the example we deal with is localized in vertex  $[\bar{T}_s; \bar{k}_r]$  of the set  $P_s$ . The minimal value of for both border values of uncertain parameter  $q$  is shown in the Table 1 also.



**Figure 4.** The spatial distribution of the cost function (23) considered in example

From Figure 4 and Table 1 the following conclusions can be formulated:

- The sensitivity of the cost function (23) on the plant uncertainty expressed by the parameter  $q$  depends on the controller gain  $k_c$ :
  - for smaller values of  $k_c$  the sensitivity is small,
  - for bigger values of gain  $k_c$  is bigger.
- For values of sample time  $T_s$  closer to maximal the cost function (23) has the minimum along the proportional gain  $k_r$ .
- For the considered case extremes of cost function are localized only in vertices of considered area of controller parameters  $P_s$ .

## Conclusions

The final conclusions from the paper can be formulated as follows:

- Results of simulations show, that the sensitivity the considered cost function on uncertainty the control plant, described by parameter  $q$  depends on the gain the controller.
- The geometric interpretation of the cost function simplifies the localization of their minimum and allows to confirm the general analytical results.
- As a subject of further considerations a deeper theoretical analysis of presented results is planned. Particularly – we plan to deal with the formulating analytical conditions describing the localization of extremes of the discussed cost function.

## References

1. Athans M, Falb PL. Optimal Control. An introduction to Theory and Its Applications, McGraw Hill 1966.
2. Isermann R. Digital Control Systems, vol. 1 Springer, 1989.
3. Isermann R. Digital Control Systems, vol. 2 Springer, 1992.
4. Mitkowski W. Stabilization of dynamical systems, WNT, 1991 (in Polish).
5. Mitkowski W, Oprzędkiewicz K. A sample time assign for a discrete interval parabolic system with the two-dimensional uncertain parameter space, Systems Science, 2004, 30, 1, 43–50.
6. Mitkowski W, Oprzędkiewicz K. A sample time optimization problem in a digital control system, System modeling and optimization 23rd IFIP TC 7 conference: Cracow, Poland, July 23–27, 2007: revised selected papers, eds. Adam Korytowski [et al.], Berlin ; Heidelberg; New York 2009.
7. Mitkowski W, Oprzędkiewicz K. A discrete minimal energy control for 2nd order uncertain-parameter plant, XVII State Conference of Automatics: Kielce–Cedzyna, 19–22.06.2011 r. Kielce University of Technology, 2011, (in Polish).
8. Mitkowski W, Oprzędkiewicz K. A minimum-energy controller for 2nd order uncertain parameter plant, Automatyka: półrocznik Akademii Górniczo-Hutniczej im. Stanisława Staszica w Krakowie, 2011, 15, 355–363.
9. Oprzędkiewicz K. Practical control of dynamic systems with point spectrum and interval parameters, AGH UST Monograph, 2008, No. 186.
10. Teneta J, Zaczyk M, Oprzędkiewicz K, Więckowski Ł, Głowacz W. Parameters identification of an oriented PV system, PAR Pomiary Automatyka Robotyka, 2012, 9, 74–79.